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## Highly efficient isopropyl alcohol removal by microwave-induced catalytic oxidation process

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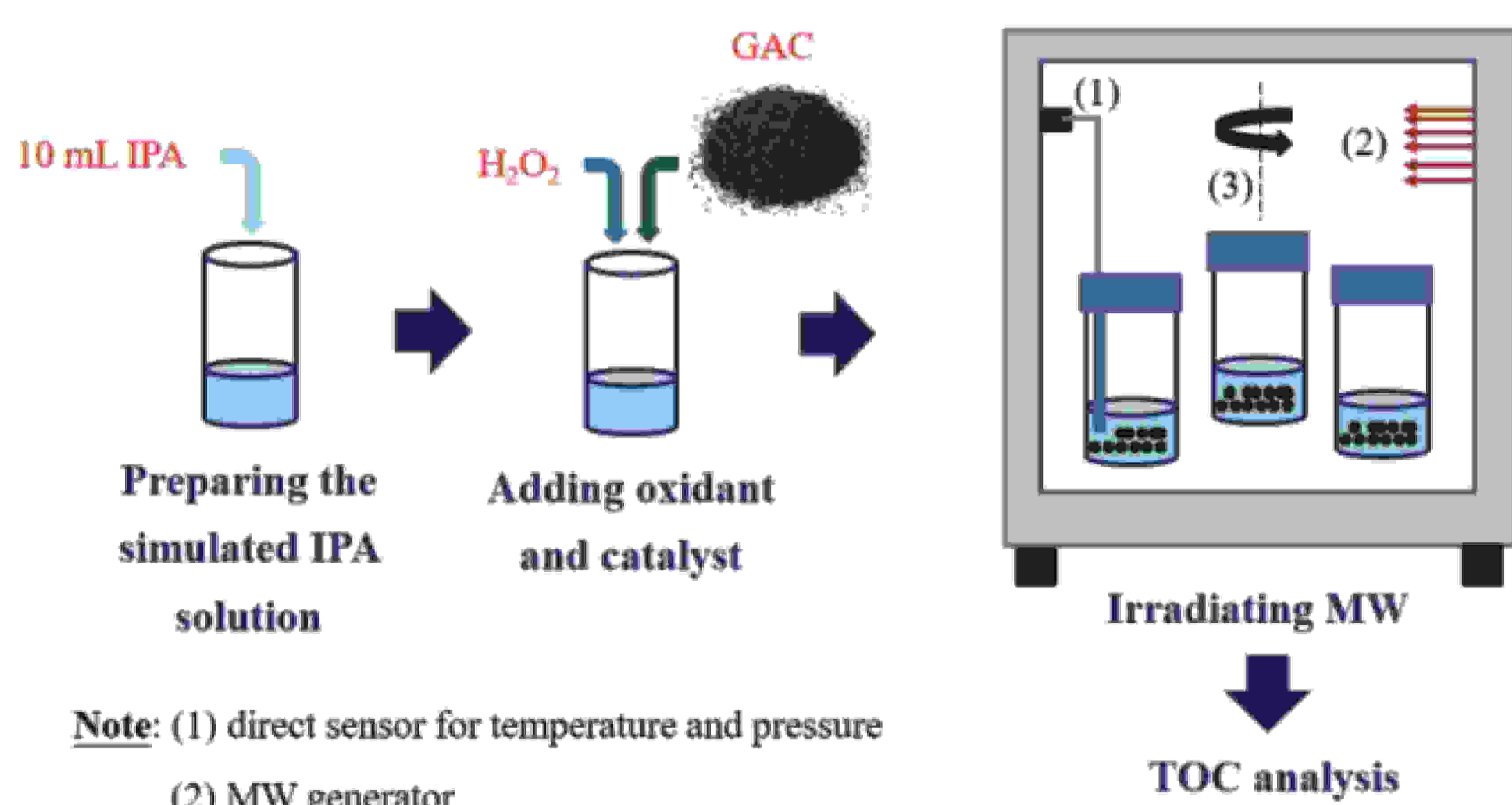
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### ABSTRACT

Isopropyl alcohol (IPA) is a common waste solvent from semiconductor and optoelectronic manufacturing industries. The current study assesses the feasibility of microwave-induced catalytic oxidation process for synthetic IPA wastewater. The effect of three independent variables, including oxidant (hydrogen peroxide), initial IPA concentration, and dosage of catalyst (granular activated carbon, GAC) on the IPA removal efficiency, were investigated and optimized by response surface methodology (RSM) based on central composite design (CCD). The estimated optimal working conditions were as follows:  $[H_2O_2] < 0.132$  M, GAC dosage = 108–123 g/L, and initial  $[IPA] = 0.038$ –0.10 M. The findings indicated that the dosage of GAC and the initial IPA concentration strongly affected the overall IPA removal. The values of  $R^2 = 0.9948$  and adjusted  $R^2 = 0.9901$  demonstrated that the response variability could be explained by the model expressing a satisfactory quadratic fit. Finally, the  $H_2O_2$ /GAC/MW process showed a faster and higher IPA removal rate than other processes tested.

### MATERIALS AND METHODS

#### a) Experimental procedure



#### b) Experimental range and levels of independent variables

Independent variables	Code	Real values of the coded levels				
		-1.682	-1	0	+1	+1.682
Concentration of $H_2O_2$ (M)	$X_1$	0.132	0.2	0.3	0.4	0.468
Dosage of GAC (g/L)	$X_2$	39.54	60	90	120	140.46
Concentration of IPA (M)	$X_3$	0.038	0.18	0.39	0.60	0.743

### RESULTS

#### 1) RSM model construction

Table 1. Design matrix by CCD, and the actual and predicted percentage TOC degradation for response surface quadratic model

Run number	Actual levels			TOC removal (%)	
	$[H_2O_2]_0$ (M)	GAC dosage (g/L)	$[IPA]_0$ (M)	Observed	Predicted
1	0.2	60	0.18	63.18	64.69
2	0.4	60	0.18	58.74	61.14
3	0.2	120	0.18	84.83	90.29
4	0.2	60	0.60	45.69	46.15
5	0.4	120	0.18	81.16	86.87
6	0.4	60	0.60	41.57	42.28
7	0.2	120	0.60	62.87	66.64
8	0.4	120	0.60	58.24	62.90
9	0.132	90	0.39	65.34	69.60
10	0.468	90	0.39	60.55	63.47
11	0.3	39.54	0.39	39.39	39.91
12	0.3	140.46	0.39	70.18	78.77
13	0.3	90	0.038	85.17	87.14
14	0.3	90	0.743	46.29	51.49
15	0.3	90	0.39	61.54	64.43
16	0.3	90	0.39	60.89	64.43
17	0.3	90	0.39	61.34	64.43
18	0.3	90	0.39	61.58	64.43
19	0.3	90	0.39	62.11	64.43
20	0.3	90	0.39	60.75	64.43

Second-order polynomial equation:

$$Y\% = 44.213 - 62.407X_1 + 0.821X_2 - 62.001X_3 + 0.011X_1X_2 - 3.810X_1X_3 - 0.203X_2X_3 + 74.439X_1^2 - 0.002X_2^2 + 39.495X_3^2$$

#### 2) Influences of the selected variables and their interactions

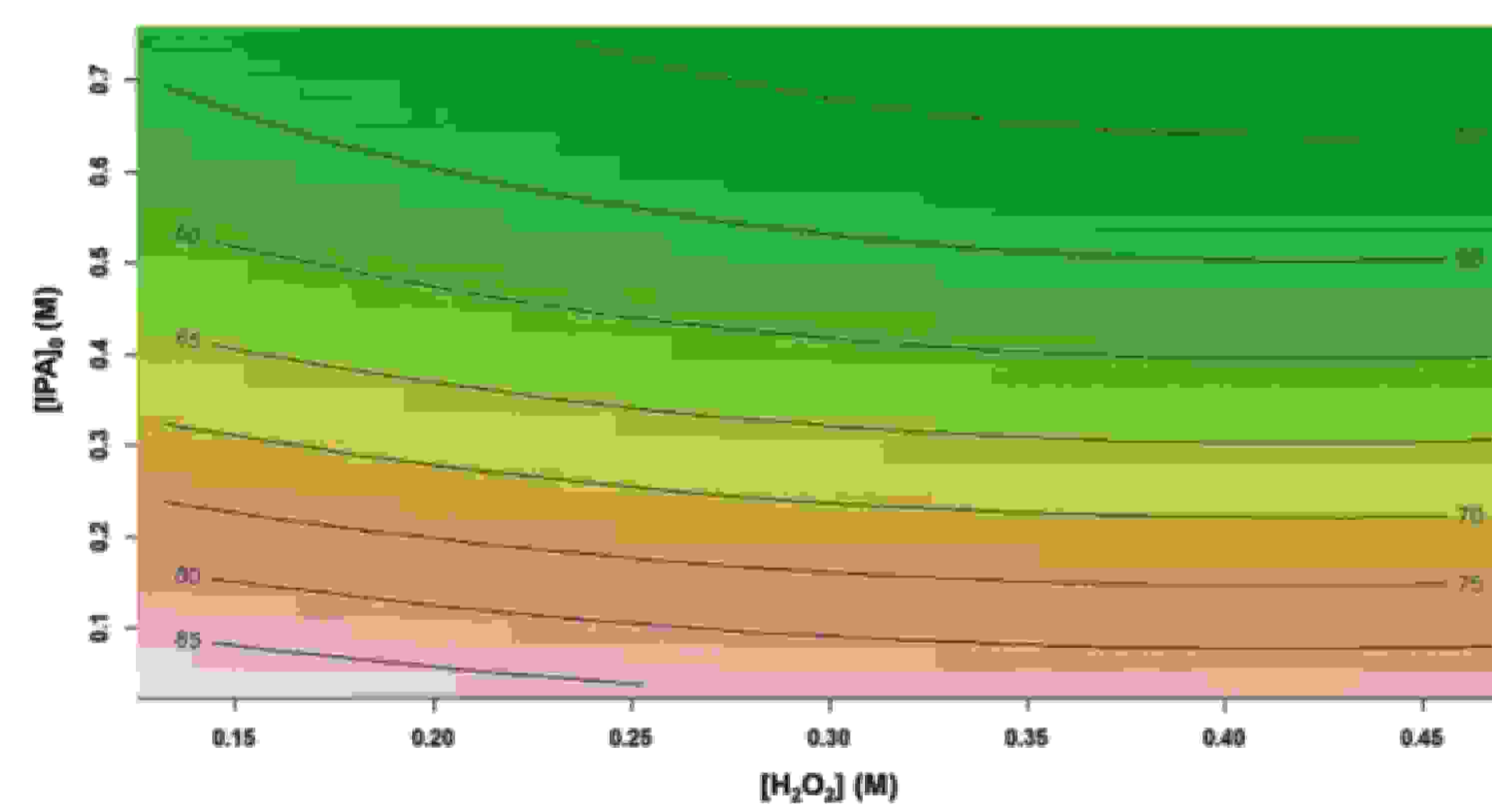


Figure 1. Influence of  $H_2O_2$  and initial IPA concentration on TOC removal. The dosage of GAC was kept at 90 g/L

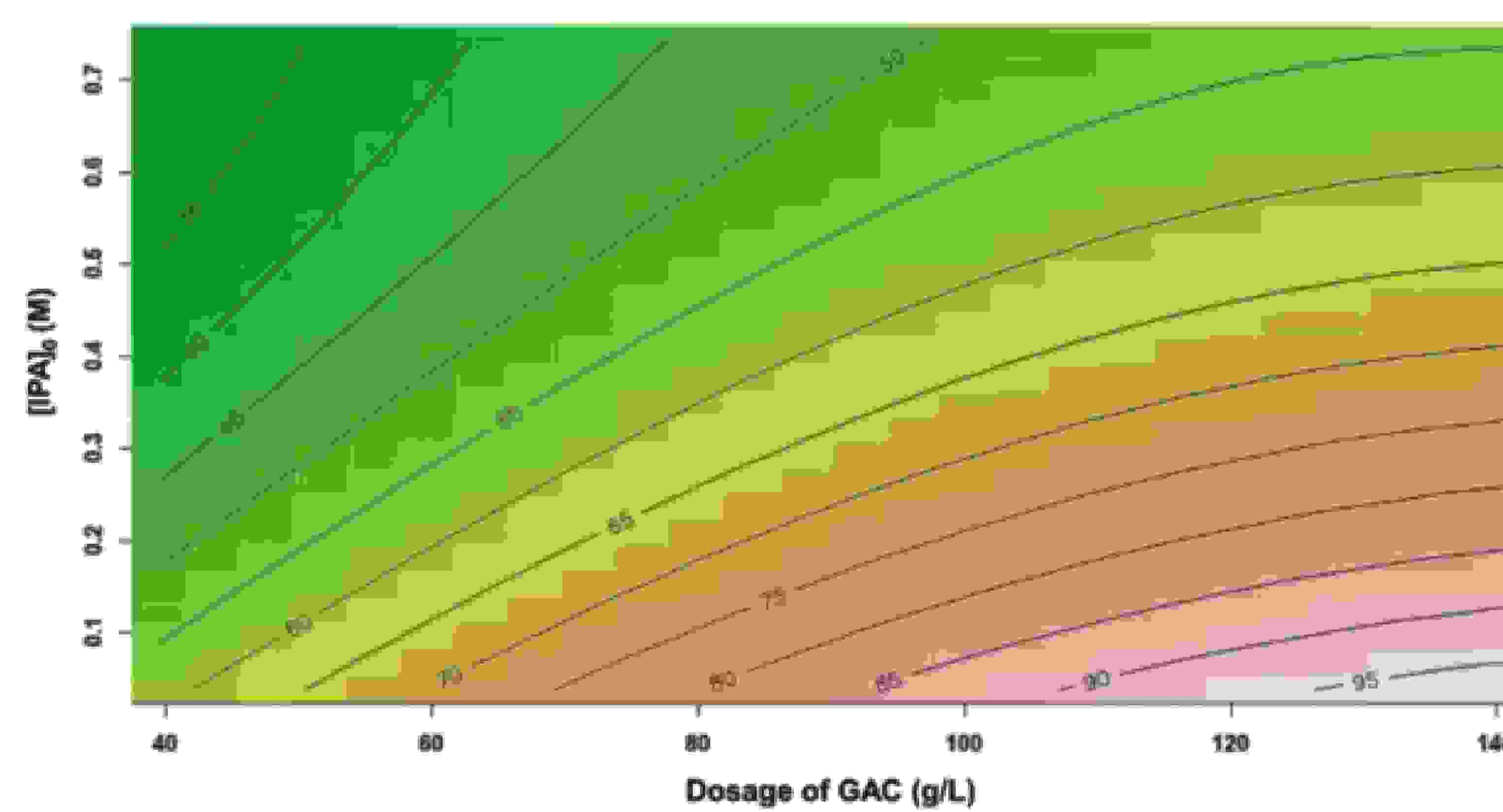


Figure 2. Influence of GAC dosage and initial IPA concentration on TOC removal. The concentration of  $H_2O_2$  was kept at 0.3 M

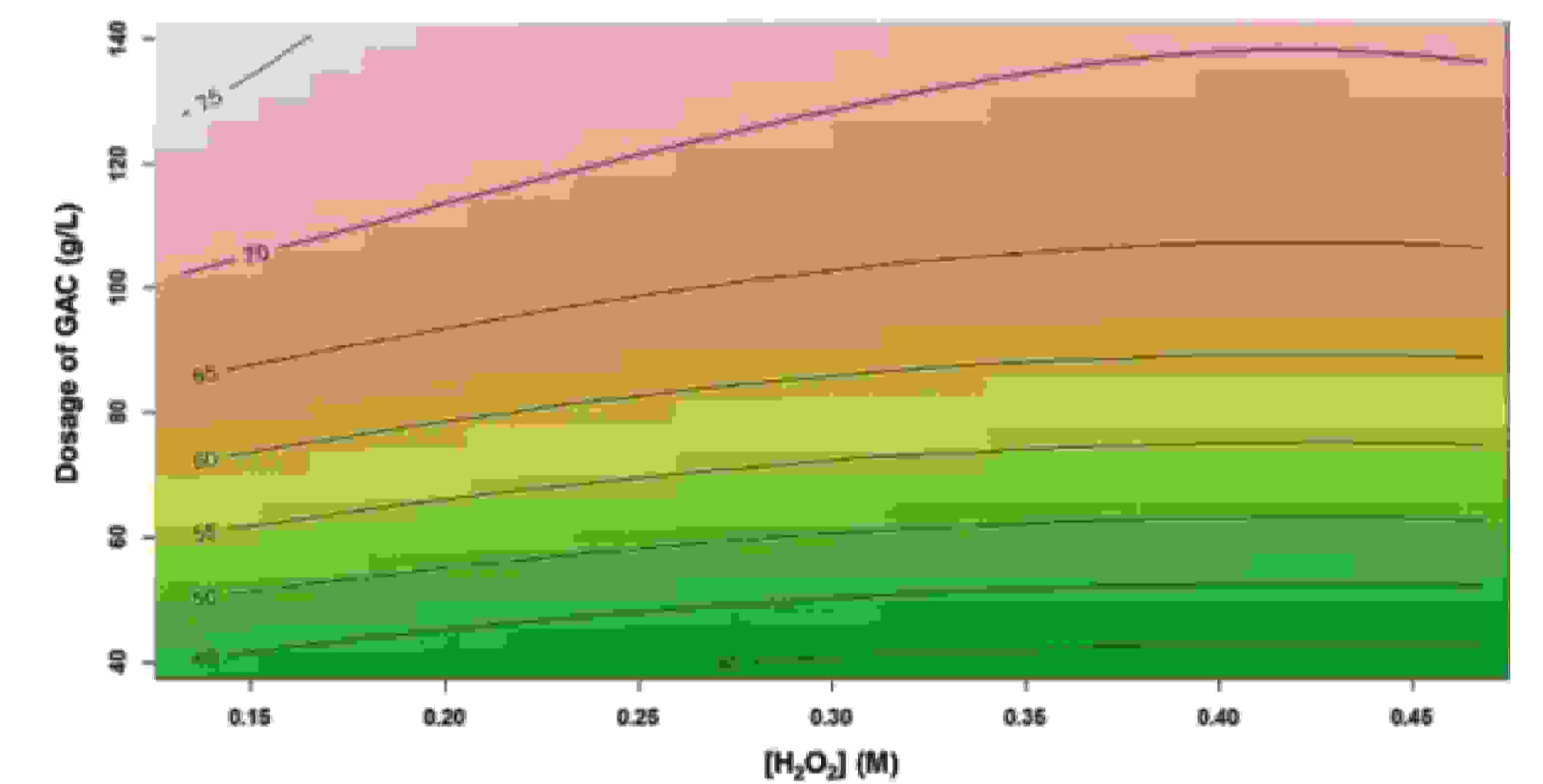


Figure 3. Influence of  $H_2O_2$  concentration and GAC dosage on TOC removal. Initial concentration of IPA was kept at 0.39 M

#### 3) Comparison of different treatment processes on TOC removal

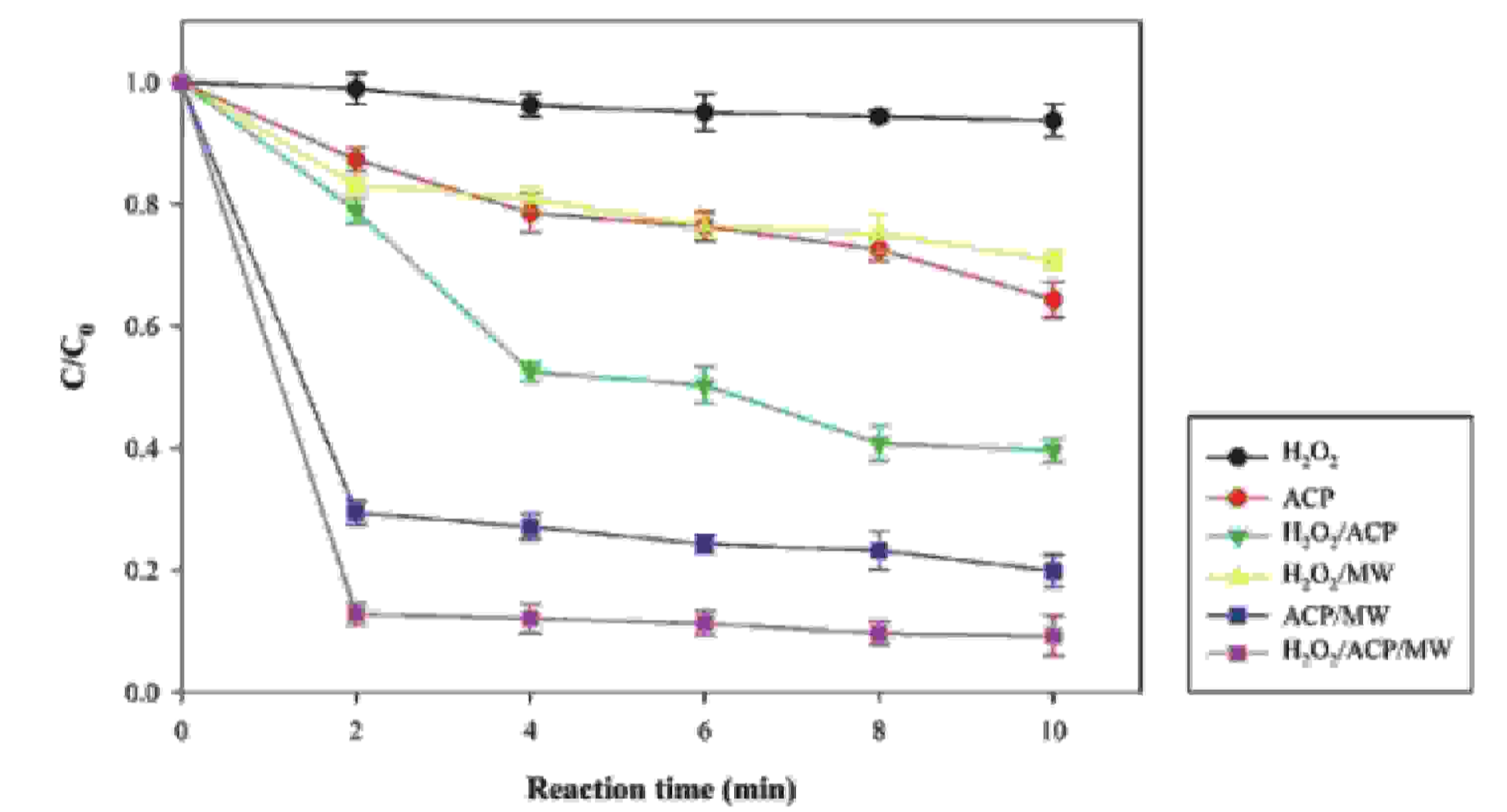


Figure 4. TOC removal by different treatment processes. Operational conditions:  $[IPA]_0 = 0.038$  M,  $[H_2O_2] = 0.132$  M,  $Q_{GAC} = 108$  g/L

#### 3) Mechanism of IPA degradation

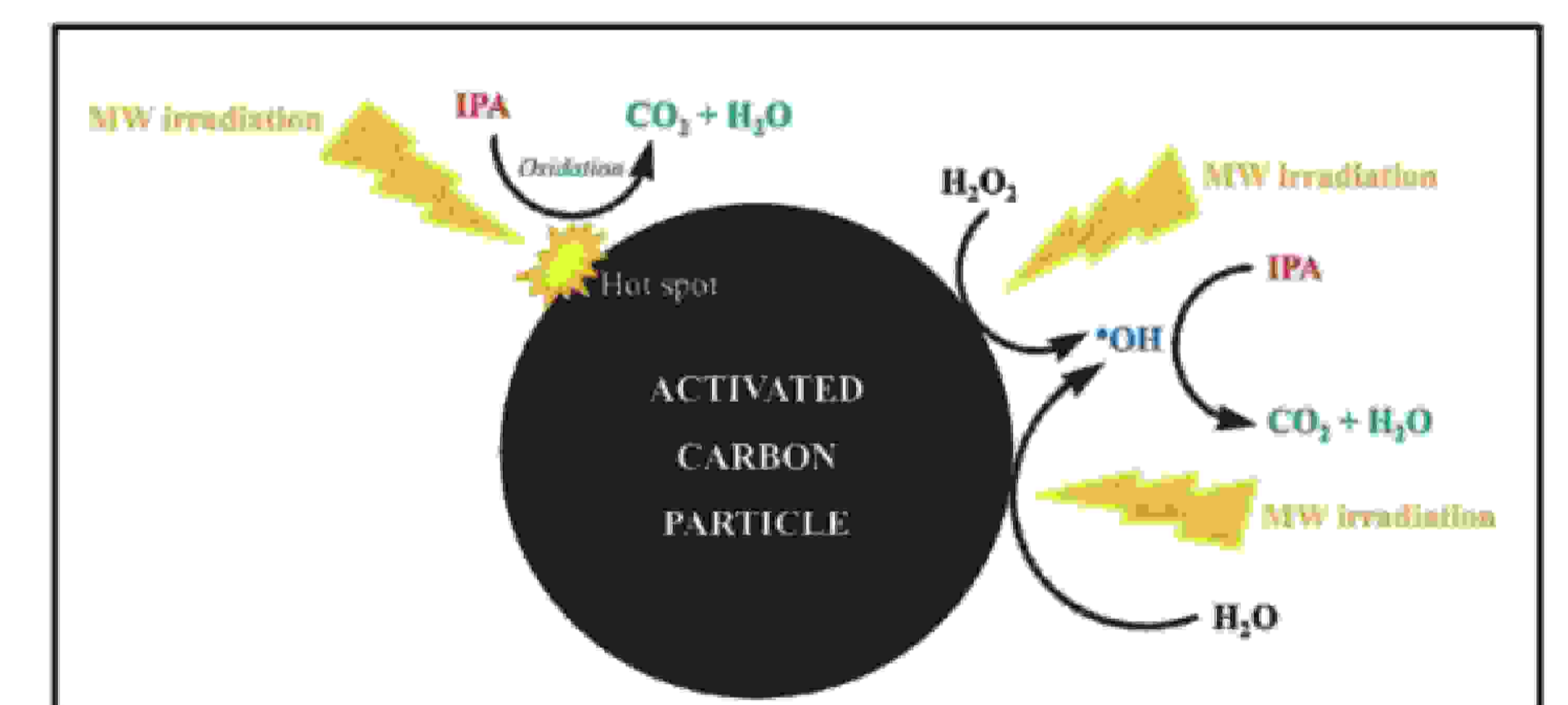


Figure 5. A proposed mechanism of IPA degradation in  $H_2O_2$ /GAC/MW combined process

### CONCLUSIONS

- TOC removal rate  $\uparrow$  as the dosage of GAC  $\uparrow$  and  $[IPA]_0 \downarrow$ . In addition, an excess of  $H_2O_2$  has a negative effect on TOC removal.
- The TOC removal efficiency reached 84.9% under optimal conditions with GAC dosage of 120 g/L,  $H_2O_2$  dosage of 0.3 M, and initial IPA concentration of 0.13 M.



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